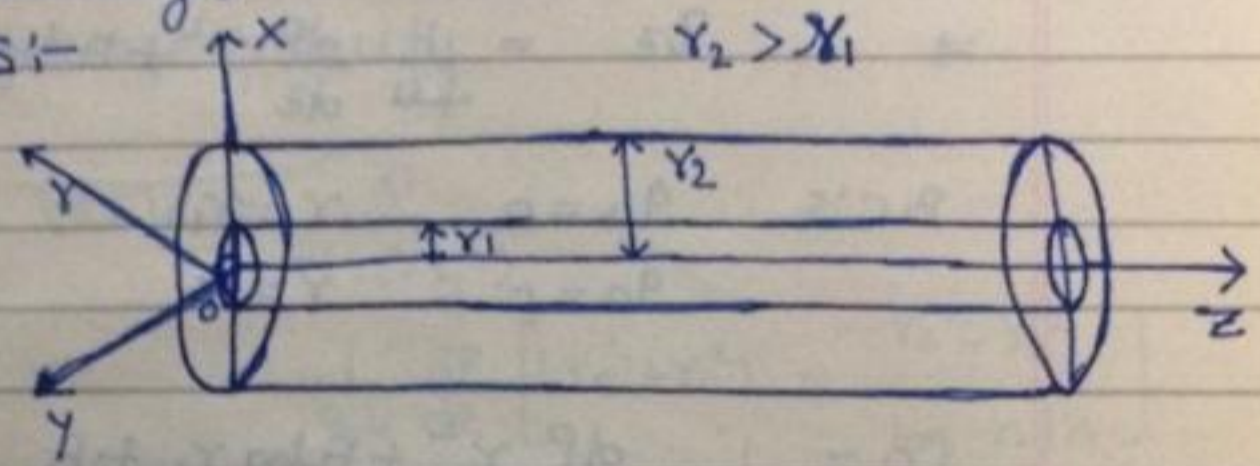


Shear stress:-

$$\begin{aligned}
 (\tau_{rz})_{r=r_0} &= -\mu \frac{dq_z}{dr} \\
 &= -\frac{1}{2} r_0 \frac{dP}{dz}
 \end{aligned}$$

Case I:- Steady flow between co-axial circular Pipes:-  $r_2 > r_1$



Consider two co-axial circular cylinder of radius  $r_1$  and  $r_2$  ( $r_2 > r_1$ ) through which laminar steady flow without body forces in incompressible fluid takes place along the axial directions.

The boundaries of both the pipes are at rest. The no slip conditions at their walls become

Equation of motion

$$0 = -\frac{\partial P}{\partial r} \Rightarrow P \text{ is Independent of } r$$

$$0 = -\frac{1}{r} \frac{\partial P}{\partial \theta} \Rightarrow P \text{ is Independent of } \theta$$

$$0 = \frac{1}{4\mu} \frac{dP}{dz} \left( \frac{d^2}{dr^2} + \frac{1}{r} \frac{d}{dr} \right) q_z$$

the Pressure  $P$  is a function of  $z$  only.

i.e.  $P = P(z)$

Average Velocity  $V = U \left( \frac{1}{2} + \frac{P}{6} \right)$

the Volumetric flow rate  $Q$  / unit width  
 $Q = Vy_0 = \left( \frac{1}{2} + \frac{P}{6} \right) Uy_0$

For maximum or minimum velocity

$\frac{dy}{dy} = 0$  we have

$\frac{dy}{dy} = \frac{U}{y_0} + \frac{U}{y_0} P \left( 1 - \frac{2y}{y_0} \right) = 0$

$= U \left[ \frac{1}{y_0} + P \left( \frac{1}{y_0} - \frac{2y}{y_0^2} \right) \right] = 0$

$\Rightarrow \frac{y}{y_0} = \frac{1}{2} \left( 1 + \frac{1}{P} \right)$

the maximum velocity  $P = 1$

$\frac{y}{y_0} = \frac{1}{2} (1 + 1)$

$\frac{y}{y_0} = 1$

$y = y_0$

For minimum velocity  $P = -1$

$\frac{y}{y_0} = \frac{1}{2} \left[ \frac{-1}{-1} - \frac{1}{1} \right]$

$\frac{y}{y_0} = 0$

It follows  $\Rightarrow$  the velocity gradient at the fixed plate is zero. it becomes negative for any value  $P < -1$

And  $0 = \frac{1}{8\mu} \frac{dP}{dx} y_0^2 - \frac{1}{2} Ay_0 + B$  — (B)

From A And B

$$B = -\frac{1}{8\mu} \frac{dP}{dx} y_0^2$$

$$A = 0$$

Substituting A And B Value in the

$$u = \frac{1}{2\mu} \frac{dP}{dx} y^2 + Ay + B$$

$$u = \frac{1}{2\mu} \frac{dP}{dx} y^2 - \frac{1}{8\mu} \frac{dP}{dx} y_0^2$$

$$u = -\frac{y_0^2}{8\mu} \frac{dP}{dx} \left( 1 - \frac{4y^2}{y_0^2} \right)$$

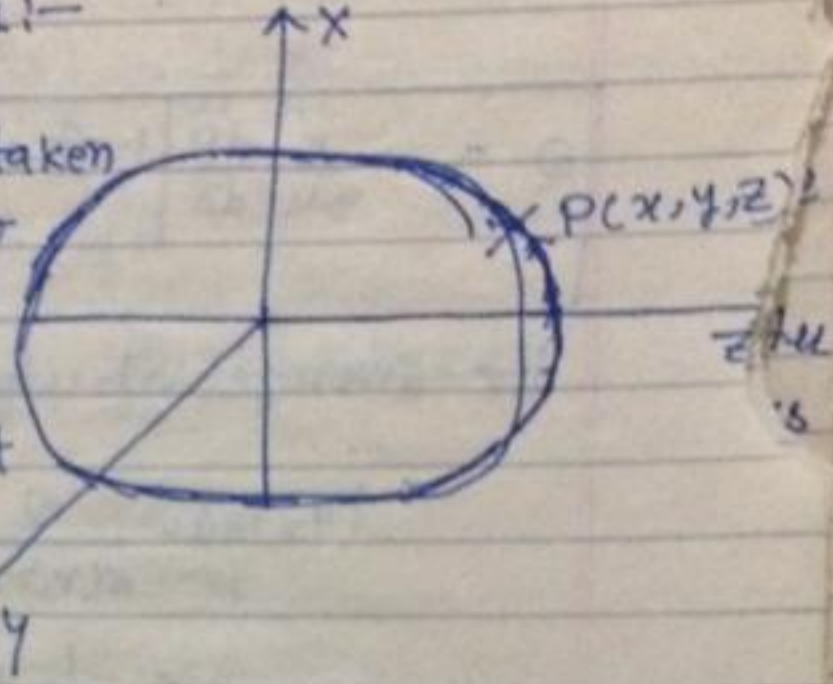
it follows that the fluid flows in the direction on the negative pressure gradient and that the velocity profile of the fully developed laminar flow between two parallel plates.

Ques:- State And Prove the Poiseuille flow between two parallel plates.

= x =

Case II Steady flow in Pipes of elliptic  
Cross-section:-

Let z-axis be taken  
 direction of flow  
 Along the axis of  
 the Pipe.  $w$  is  
 velocity component  
 velocity component  
 $w$  is indepen  
 dent  $z$



the Equation of continuity

$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} + \frac{\partial w}{\partial z} = 0$$

Velo. comp.

$$u = 0, v = 0, w = w(x, y) \quad \text{--- (1)}$$

$$\frac{dw}{dz} = 0 \Rightarrow w \text{ is independent } z$$

the NSE

$$0 = -\frac{\partial p}{\partial x} \quad \text{--- (2)}$$

$$0 = -\frac{\partial p}{\partial y} \quad \text{--- (3)}$$

$$0 = -\frac{\partial p}{\partial z} + \mu \left( \frac{\partial^2 w}{\partial x^2} + \frac{\partial^2 w}{\partial y^2} \right) \quad \text{--- (4)}$$

Differentiating the equation (4) with  
 regard to  $z$ , we have

$$\frac{d^2 p}{dz^2} = 0$$

$$\Rightarrow \frac{dp}{dz} = \text{const.} = -c$$

the Pressure gradient

$$\frac{dP}{dz} = \frac{P_2 - P_1}{L}$$

$$q_z = -\frac{\lambda_0^2}{4\mu} \frac{P_2 - P_1}{L} \left(1 - \frac{r^2}{\lambda_0^2}\right)$$

Where  $P_1$  and  $P_2$  are Pressure  
Maximum velocity

$$(q_z)_{\max} = -\frac{\lambda_0^2}{4\mu} \frac{dP}{dz}, \quad \frac{dP}{dz} < 0$$

$$\frac{q_z}{(q_z)_{\max}} = 1 - \frac{r^2}{\lambda_0^2}$$

this is known as Hagen-Poiseuille flow

Average velocity

$$(q_z)_{\text{av}} = \frac{1}{\pi \lambda_0^2} \int_0^{2\pi} \int_0^{\lambda_0} q_z r dr d\theta$$

$$\Rightarrow (q_z)_{\text{av}} = \frac{1}{\pi \lambda_0^2} \int_0^{2\pi} \int_0^{\lambda_0} -\frac{\lambda_0^2}{4\mu} \frac{dP}{dz} \left(1 - \frac{r^2}{\lambda_0^2}\right) r dr d\theta$$

$$\Rightarrow (q_z)_{\text{av}} = -\frac{1}{2\mu} \frac{dP}{dz} \left(\frac{1}{2} \lambda_0^2 - \frac{1}{4} \lambda_0^2\right)$$

$$= \frac{1}{2} \left(-\frac{\lambda_0^2}{4\mu} \frac{dP}{dz}\right)$$

$$= \frac{1}{2} (q_z)_{\max}$$

the volumetric flow  $Q$

$$Q = \frac{1}{2} (q_z)_{\max} \pi \lambda_0^2$$

$$Q = -\frac{\pi \lambda_0^4}{8\mu} \frac{dP}{dz}$$